In the Claims:

Please amend the claims as follows.

1. (Currently Amended) A process for making multiple grades of base oil products, wherein said process comprises the following steps:

(a) hydrocracking a mineral crude derived feed, thereby obtaining an effluent;

(b) distilling of the effluent as obtained in step (a) into at least one middle distillates product and a full range residue boiling substantially above 340 °C;

(c) catalytically dewaxing the full range residue by contacting the full range residue with a dewaxing catalyst comprising a dealuminated extrudate of a zeolite of the MTW type and a low acidity refractory binder material wherein the weight ratio of said zeolite to said low acidity refractory binder material is in the range of from 5:95 to 95:5 and a Group VIII metal of either platinum or palladium that is present in said dewaxing catalyst in the range of from 0.1 to 5.0% by weight, thereby obtaining a dewaxed oil;

(d) isolating by means of distillation two or more base oil grades from the dewaxed toil obtained in step (c); and

(e) isolating a dewaxed gas oil from the dewaxed oil obtained in step (c);

wherein the dewaxed oil as obtained in step (c) comprises between 10 and 40 wt% of a dewaxed heavy gas oil boiling for more than 70 wt% between 370 and 400 °C.

2. (Previously Presented) The process according to claim 1, wherein more than 20 wt% of the mineral crude derived feed to step (a) boils above 470 °C.

3. (Previously Presented) The process according to claim 2, wherein a fraction of the dewaxed gas oil is recycled to step (b) to be mixed with the effluent before distilling thereof.

4. (Previously Presented) The process according to claim 3, wherein from 0 to 15 wt% of the full range residue as obtained in step (b) is recycled to step (a) to be mixed with the mineral crude derived feed before hydrocracking thereof.

5. (Previously Presented) The process according to claim 4, further comprising adding a Fischer-Tropsch derived partly isomerised paraffin fraction to the full range residue prior to catalytically dewaxing.

6. (Currently Amended) The process according to ~~any one of~~ claim 5, wherein the dewaxed oil of step (c) is subjected to an additional hydrofinishing step.

7. (Previously Presented) The process according to claim 6, wherein the hydrogen partial pressure in step (c) is greater than 100 bars.

8. (Currently Amended) The process according to claim~~s~~ 7, wherein the base oil grades obtained in step (d) each comprises more than 95 wt% saturates and have a viscosity index of between 95 and 120.

9. (Previously Presented) A dewaxed gas oil made by the process of claim 1.

10. (Previously Presented) A dewaxed gas oil according to claim 9, wherein the gas oil has an aromatic content of below 0.1 mmol/100 grams, a sulphur content of below 10 ppm and a pour point of below –30 °C.

11. (Canceled)